Reply to Office Action of November 13, 2007

AMENDMENTS TO THE CLAIMS

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This listing of claims will replace all prior listings and versions thereof.

Claims 1-14. (cancelled)

Claim 15. (previously presented) A device for introducing gas into a fluidized bed comprising:

at least one gas inlet pipe located underneath and/or above the fluidized bed, wherein the gas inlet pipe has gas-swirling means at its mouth, the gas-swirling means comprising at least one bead.

Claim 16. (cancelled)

Claim 17. (previously presented) A device of claim 16 wherein the narrowing has at least one edge.

Claim 18-20. (cancelled)

Claim 21. (previously presented) A device of claim 15 wherein the gas comprises ethene, oxygen and/or hydrogen chloride.

Claim 22. (previously presented) A fluidized reactor bed comprising a device of claim 15.

Claim 23. (previously presented) A process for the production of 1,2-dichloroethane with a fluidized bed reactor comprising a device for introducing gas, the method comprising:

introducing ethene, oxygen and/or hydrogen chloride into a fluidized bed comprising a catalyst,

wherein the device comprises at least one gas inlet pipe located underneath and/or above the fluidized bed and the gas inlet pipe has gas-swirling means at its mouth, the gas-swirling means comprising at least one bead.

Claim 24. (previously presented) The process of claim 23 wherein the gas inlet pipe is arranged underneath the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 0.5 to 10 m/s.

Claim 25. (previously presented) The process of claim 23 wherein the gas inlet pipe is arranged underneath the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 3 to 6 m/s.

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Claim 26. (previously presented) The process of claim 23 wherein the gas inlet pipe is arranged above the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 0.7 to 10 m/s.

Claim 27. (previously presented) The process of claim 23 wherein the gas inlet pipe is arranged above the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 2 to 5 m/s.

Claim 28. (previously presented) A device of claim 15 wherein the at least one bead has at least one edge.

Claim 29. (previously presented) A device of claim 28 wherein the at least one edge is a sharp edge.

Claim 30. (previously presented) A device of claim 15 wherein the at least one bead is an annular bead arranged at least part of an inner circumference of the gas inlet pipe.

Claim 31. (previously presented) A device for introducing gas into a fluidized bed comprising:

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at least one gas inlet pipe located underneath and/or above the fluidized bed, wherein the gas inlet pipe has gas-swirling means at its mouth, the gas-swirling means comprising at least one screen, at least one turbulence grid and/or at least one perforated diaphragm.

Claims 32-35. (cancelled)

Claim 36. (previously presented) A device of claim 31 wherein the gas comprises ethene, oxygen and/or hydrogen chloride.

Claim 37. (previously presented) A fluidized reactor bed comprising a device of claim 31.

Claim 38. (previously presented) A process for the production of 1,2-dichloroethane with a fluidized bed reactor comprising a device for introducing gas, the method comprising:

introducing ethene, oxygen and/or hydrogen chloride into a fluidized bed comprising a catalyst,

wherein the device comprises at least one gas inlet pipe located underneath and/or above the fluidized bed and the gas inlet pipe has gas-swirling means at its mouth, the

gas-swirling means comprising at least one screen, at least one turbulence grid and/or at least one perforated diaphragm.

Claim 39. (previously presented) The process of claim 38 wherein the gas inlet pipe is arranged underneath the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 0.5 to 10 m/s.

Claim 40. (previously presented) The process of claim 38 wherein the gas inlet pipe is arranged underneath the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 3 to 6 m/s.

Claim 41. (previously presented) The process of claim 38 wherein the gas inlet pipe is arranged above the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 0.7 to 10 m/s.

Claim 42. (previously presented) The process of claim 38 wherein the gas inlet pipe is arranged above the fluidized bed and the gas current is discharged at an average discharge velocity in the range of from 2 to 5 m/s.